

$$l(t=0) = l_0$$

$$[x_i](t=0) = [x_i]_0$$

$$\int_{t_0}^{t_1} dt$$

$$\frac{dT}{dt} = \frac{\dot{Q}N - \sum_i \bar{h}_i \dot{\omega}_i}{\sum_i (N_i) \bar{c}_{p,i}} \quad \begin{matrix} \text{Const P} \\ \text{Fixed mass} \end{matrix}$$

$$\frac{d[x_i]}{dt} = \dot{\omega}_i - [x_i] \left(\frac{\sum_i \dot{\omega}_i}{\sum_i [x_i]} + \frac{dT}{dt} \right)$$

$$\begin{matrix} V = \text{const.} \\ m = \text{const.} \end{matrix}$$

$$m \frac{du}{dt} = \dot{Q}_m - \dot{W}_m + \sum_i \dot{E}_i - \sum_i \dot{E}_i$$

$$\frac{du}{dt} = \frac{\dot{Q}}{m}$$

$$\rightarrow \frac{dT}{dt} = \frac{(\dot{Q}N) - \sum_i (\bar{u}_i \dot{\omega}_i)}{\sum_i (N_i) \bar{c}_{v,i}}$$

$$\bar{u}_i = \bar{h}_i - R_0 T \quad \bar{c}_{v,i} = \bar{c}_{p,i} - R_0$$

$$\frac{dT}{dt} = \frac{(\dot{Q}N) + R_0 T \sum_i \dot{\omega}_i - \sum_i (\bar{h}_i \dot{\omega}_i)}{\sum_i (N_i) (\bar{c}_{p,i} - R_0)}$$

need $\frac{dP}{dt}$ for const. V

$$VP = \sum_i N_i R_0 T$$

$$P = \sum_i [x_i] R_0 T$$

$$\frac{dP}{dt} = R_0 T \sum_i \frac{d[x_i]}{dt} + R_0 \sum_i [x_i] \frac{dT}{dt}$$

$$\dot{\omega}_i = \frac{d[x_i]}{dt} + \frac{[x_i]}{V} \frac{dV}{dt} = \frac{d[x_i]}{dt}$$

$$\left[\frac{dP}{dt} = R_0 T \sum_i \dot{\omega}_i + R_0 \sum_i [x_i] \frac{dT}{dt} \right]$$

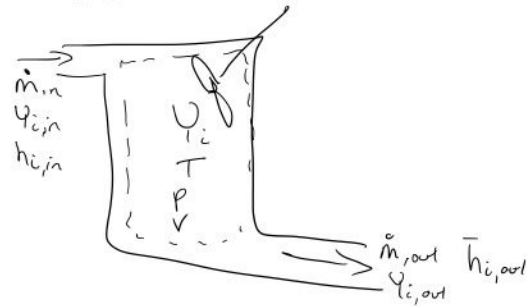
$$\frac{dT}{dt} = f([x_i], T)$$

$$\frac{d[x_i]}{dt} = \dot{\omega}_i = f([x_i], T)$$

$$T(t=0) = T_0$$

$$[x_i](t=0) = [x_i]_0$$

Well-Stirred Reactor



mass:

$$\frac{d m_{i,cv}}{dt} = \dot{m}_{i,in} - \dot{m}_{i,out} + \dot{m}_i^{\text{gen}} V$$

$$\frac{dm}{dt} = \dot{m}_m - \dot{m}_{out}$$

$$\dot{m}_i^{\text{gen}} = \dot{\omega}_i m_{w,i}$$

$$\dot{m}_i = \dot{m} Y_i \quad (\text{no diffusion})$$

SS.

$$0 = \dot{w}_i MW_i V + \dot{m} (Y_{i,in} - \underline{Y_{i,out}})$$

$$Y_i = \frac{[x_i] MW_i}{\sum_i [x_i] MW_i}$$

energy:

$$\frac{d\dot{w}}{dx} = \dot{E}_{in} - \dot{E}_{out} + \dot{Q} - \dot{w}$$

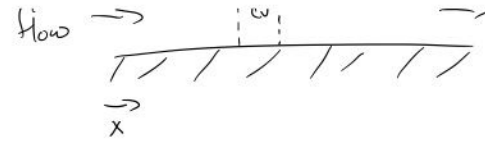
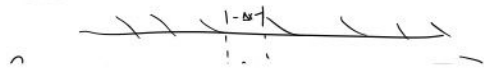
$\dot{m} h_{in}$ $\dot{m} h_{out}$

$$\dot{Q} = \dot{m} (h_{out} - h_{in})$$

residence time:

$$t_R = \frac{\rho V}{\dot{m}} \frac{[kg]}{[kg/s]} = [\text{time}]$$

Plug Flow Ret



1) SS.

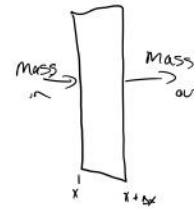
2) no axial mixing

3) 1-D flow (uniform properties perpendicular to flow)

4) ideal frictionless flow

5) ideal gas

Mass balance:



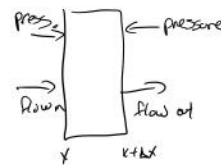
$$\dot{m} = \rho V_x A$$

$$(\rho V_x A)_x - (\rho V_x A)_{x+dx} = 0$$

$\Delta x \rightarrow 0$

$$\frac{d}{dx} (\rho V_x A) = 0$$

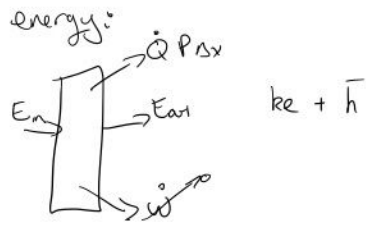
X-momentum



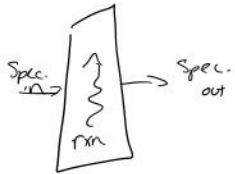
$$\text{acc. } \dot{m} \frac{dV}{dt} = \text{mom. flow in-out} - \text{mom. forces}$$

e.g. $(PA)_x$

$$(PA)_{x+dx} = (PA)_x + \frac{d}{dx} (PA) dx$$



Species



$$\frac{dm_i}{dt} = \dot{m}_{i,in} - \dot{m}_{i,out} + \dot{m}_{gen}$$

$$\dot{m}_{gen} = \dot{m}_i'' A dx = \dot{w} M W_i A dx$$

mass: $\frac{d(\rho v_x A)}{dx} = 0$

momentum: $\frac{dP}{dx} + \rho v_x \frac{dv_x}{dx} = 0$

energy: $\frac{d(h + v_x^2/2)}{dx} + \frac{\dot{Q}' P_{rxn}}{m} = 0$

species: $\frac{dY_i}{dx} - \frac{\dot{w}_i M W_i}{\rho v_x} = 0$